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# **Bio-failure or Bio-fuel? Economic Feasibility of Converting Palm Oil Waste to Biogas**

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**Abstract.** This study aimed to investigate the economic feasibility of using an Up-Flow Anaerobic Sludge Blanket (UASB) reactor to convert liquid waste from palm oil processing plants into biogas containing methane. The study examined total capital investment (TCI), working capital investment (WCI), and production costs at different capacities (3, 30, and 300 liters per day) to determine if the process could generate a profit. The results showed that the biogas production from palm oil industrial liquid waste using the UASB reactor did not result in a profit due to the large capital costs and low biogas production. The implication of this study is that further research is needed to find ways to reduce the capital costs of the process and increase biogas production to make it economically feasible.

Keywords: techno-economic assessment, biogas, Up-Flow Anaerobik Sludge Blanket reactor

#### **1** Introduction

It was reported that in 2021 Indonesia has around 14,663.6 hectares of oil palm plantations [1]. Palm oil is a strength industrial plant for the Indonesian economy and is one of the plantation commodities that contributes a large foreign exchange. Refinitiv Agricultural Research reported that in 2021 global palm oil demand increased around 6.5%, from 47.6 to 50.6 million tonnes[2]. The increase in demand of palm oil triggers an increase in the area of oil palm plantations and encourages the growth of palm oil plants that produce CPO. Palm oil plant produces around 20-23% of Crude Palm Oil (CPO), 5-7% of kernel and the remaining around 70-75% is a waste [3]. To date, the processing of palm oil waste has only been based on the fulfillment of waste quality standards without further utilization of the economic values that can be generated from the waste.

Fossil energy sources are limited, hence biogas as a renewable energy source has potential to be produced. Liquid waste from palm oil processing plants contains organic and inorganic compounds, with the help of microbes in the anaerobic process it can be converted into biogas. In biogas production, the process of decomposition of organic substances by bacteria follows 2 stages i.e acetogenesis and methanogenesis [3].

There are many types of anaerobic reactors that can be used for wastewater treatment, UASB is an anaerobic digester that is widely used to treat various types of industrial wastewater due to its capacity is greater than others. UASB reactor has the ability to treat wastewater with a high organic matter load, addition it can produce biogas. High concentration of anaerobic microorganisms because

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microorganisms are combined into solid granules then produce higher methane [4].  $CH_4$  or methane is the main component of biogas which has a fairly high heating value.

In this work, a techno-economic assessment (TEA) at the early stage of biogas production from palm oil industrial liquid waste using up-flow anaerobik sludge blanket reactor is made by estimating total production cost and profit. The experimentally determined UASB reactor performance, different scenarios as capacity, the CAPCOST program, and cost data available in the literature were used to estimate the cost of the equipments.

The upflow anaerobic sludge blanket (UASB) reactor is one of the anaerobic continuous reactors which was developed in the 1970s by Lettinga and his coworkers [5]. The UASB reactor is a widely used for treating high-strength industrial wastewater. Many efforts have also been made to improve the "gas solid liquid" separation inside the bioreactor in order to avoid the loss of fine biomass particles, addition anaerobic reactors could be used to produce biogas by treating wastewaters [6]. In the UASB reactor, at the bottom of the reactor is an anaerobic sludge in the form of suspended granules and wastewater flows upward through the mud blanket. In the UASB reactor, the processes of acidogenesis and methanogenesis are separated so as to improve reactor performance and assist in biomass retention, further enabling the recovery of biomass during hydraulic and organic shocks [7]. UASB reactor has a low cost, operational simplicity, low sludge production , besides the cost for operation and maintenance of a UASB reactor requires less than 1% of its capital cost per year [8],[9].

# 2 Methodology

The TEA model is developed using expererimental data in order to perform the TEA of UASB reactor in converting liquid waste of palm oil processing plant into biogas [3]. Fig. 3.1 presents the working process of UASB reactor. TEA analysis to assess the economic feasibility using the following assumptions and equations. Total capital investment (TCI) is the cost acquired to set up and operate the plant which is calculated from fixed and working capital investment (FCI and WCI). FCI is the total cost of installing process equipment, buildings and tools while WCI consists of raw material, in-process, product, extended credit and available cash inventories. WCI also can be calculated around 10–15% of the TCI or 25% of the annual production selling values [10]. Total production cost (TPC) is the amount of Direct, Indirect, Fixed Manufacturing Costs and General Expenses (GE) [10],[11]. There are three scenarios of reactor capacity i.e a reactor capacity of 3.3 liter/day, 30 liter/day and 300 liter/day with incubation period of 10-12 days. The factory is estimated at 10 years with an annual depreciation of 10%, operated for 330 days per year [11], labor costs is estimated 10% of total sales.

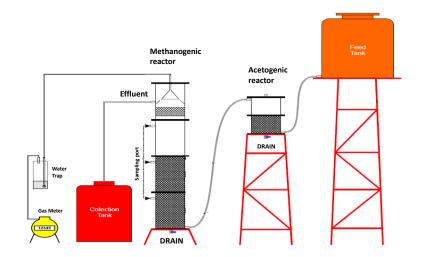


Fig.1. The working process of UASB reactor.

# **3** Result and Discussion

Total capital investment and production cost [11] at different capacities are shown in Table 1 and Table 2. The price of biomethane is assumed of 1.23 USD or Rp 18,163per litre [12].

Table 1. Total capital Investment at different biogas productions.				
Description	Production capacity of biogas			
	3 L/day	30 L/day	300 L/day	
Support from iron; cast concentrate for 30	10,000,000			
and 300 L/day				
Feed tank 1200 L from plastic, cast concentrate for 30 and 300 L/day	2,000,000	8,352,000	43,772,000	
Circulation tank 600 L from plastic, cast concentrate for 30 and 300 L/day	1,000,000	6,057,000	20,799,000	
Acedogenic reactor	5,000,000	45,000,000	450,000,000	
Methanogenic reactor	2,000,000	18,000,000	180,000,000	
Perilstatic pump	15,000,000	135,000,000	1,215,000,000	
Water scrubber	2,000,000	18,000,000	180,000,000	
Gas measurement	2,000,000	2,000,000	2,000,000	
Purchasing cost			34,500,000	
Installing process	8,625,000	44,375,000	405,500,000	
Fixed Capital Investment (FCI)	43,125,000	414,384,000	3,715,671,000	
Working Capital Investment (WCI = 10% TCI)	4,791,666	46,042,667	412,852,333	
Total cost investment (TCI)	47,916,667	460,426,667	4,128,523,333	

 Table 1. Total capital Investment at different biogas productions.

Table 1 describes that fixed capital cost (FCI) contributes around 90% of total cost invesment (TCI). This is due to several reactors and huge feed tank needed for producing biogas using UASB reactor. Table 2 shows that the production of biogas from liquid waste of palm oil plant using UASB reactor does not provide financial benefits. This is because the liquid waste processed is quite large so it requires a large investment but the production of biogas is still low (see Table 1).

I able 2. Total production cost at different biogas productions.				
Description	Production capacity of biogas			
	3 L/day	30 L/day	300 L/day	
Labor (L)	1,798,178	17,981,776	179,817,759	
Maintenance (1% FCI)	431,250	4,143,840	37,156,710	
Utilitas	17,820,000	178,200,000	1,782.000,000	
Direct Manufacturing Cost (DMC)	20,049,428	200,325,615	1,998,974,469	
Laboratory (10% L)	179,817	1,798,177	17,981,775	
Indirect Manufacturing Cost (IMC)	179,817	1,798,177	17,981,775	
Depreciacion (10%FCI)	4,312,000	41,438,400	371,567,100	
Fixed manufacturing cost (FMC)	4,312,000	41.438,400	371,567,100	
Manufacturing cost (MC)	24,541,745	243,562,193	2,388,523,345	
Administration (3%MC)	736,252	7,306,865	71,655,700	
R&D Cost (3,5% MC)	858,961	8,524,676	83,598,317	
General expense (GE)	1,595,213	15,831,542	155,254,017	
Total production cost (TPC) = MC +	26,136,959	259,393,736	2,543,777,362	
GE)				
Sales (Rp 18,163 / L)	17,981,775	179,817,759	1,798,177,590	
Profit	-8,155,184	-79,575,977	-745,599,772	

Table 2. Total production cost at different biogas productions

In the processing of liquid waste, it will reduce environmental pollution, both water and soil. In the operation of industrial wastewater treatment plants produce direct emissions due to biological processes, greenhouse gases (GHG) such as carbon dioxide (CO2), methane (CH4), and nitrous oxide (N2O), in addition to indirect emissions resulting from energy generation [13]. Treatment of wastewater into biogas is one possible way to reduce these emissions. By processing palm oil effluent, the quality of the environment is getting better, such as a reduction in greenhouse gas emissions that is causing a global warming. Hence, for further TEA studies, it is necessary to study the environmental, health and social impacts of waste treatment which are converted into economic values.

### 4 Conclusion

Biogas can be produced by treating the palm oil industrial liquid waste using up-flow anaerobik sludge blanket reactor (UASB reactor). In this study, TEA analysis showed that the production of biogas for capacities of 3.3, 30 and 300 liters per day using UASB reactor did not provide a profit. However, with this waste treatment, the quality of the environment and public health is getting better. Therefore, in TEA assessment, analysis of environmental impacts, social and public health should be considered in the economic calculation. This comprehensive analysis will be interesting if the process of converting liquid waste into biogas is integrated with a Crude Pal Oil plant where the energy produced is used for plant operations.

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